

Docket No. 0365-0501P

REMARKS

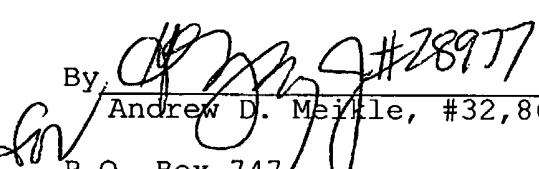
The specification has been amended to provide a cross-reference to the previously filed International Application. The claims have also been amended to delete improper multiple dependencies and to place the application into better form for examination. Entry of the present amendment and favorable action on the above-identified application are earnestly solicited.

Attached hereto is a marked-up copy of the changes made to the application by this Amendment.

If necessary, the Commissioner is hereby authorized in this, concurrent, and future replies, to charge payment or credit any overpayment to Deposit Account No. 02-2448 for any additional fees required under 37 C.F.R. § 1.16 or under 37 C.F.R. § 1.17; particularly, extension of time fees.

Respectfully submitted,

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Attachment: Version With Markings Showing Changes Made

(Rev. 01/22/01)

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VERSION WITH MARKINGS SHOWING CHANGES MADE

The specification has been amended to provide cross-referencing to the International Application.

The claims have been amended as follows:

6. (Amended) The method according to [any of claims 2 to 5]claim 2, wherein the control valve is adjusted to provide for pulsating operation to prevent clogging of the valve.

7. (Amended) The method according to [any of the preceding claims]claim 1, wherein polymer powder is continuously withdrawn from a point above a fluidization plate.

8. (Amended) The method according to [any of the preceding claims]claim 1, wherein polymer powder is continuously withdrawn from a point below the bed level.

9. (Amended) The method according to [any of the preceding claims]claim 11, wherein the discharge line and the control valve are discontinuously backflushed with a flushing gas flow.

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10. (Amended) The method according to [any of the preceding claims]claim 1, comprising

- using a gas phase reactor having a mechanically mixed zone of the fluidized bed, and
- continuously withdrawing polymer powder from said mixed zone.

11. (Amended) The method according to [any of the preceding claims]claim 1, wherein polymer powder is also separately withdrawn from the reactor using a discontinuous discharge device.

12. (Amended) The method according to [any of the preceding claims]claim 1, wherein the polymer powder is withdrawn together with gas from the reactor, the gas is separated from the polymer powder, and the separated gas is recycled into the reactor.

13. (Amended) The method according to [any of the preceding claims]claim 1, wherein polymer agglomerates are withdrawn from the reactor using a discharge line with a discontinuously operated discharge valve.

19. (Amended) The method according to [any of the preceding claims]claim 1, wherein the catalyst is fed into the gas phase reactor as a stream comprising polymer and active catalyst together with reaction medium.

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22. (Amended) The method according to [any of the preceding claims]claim 1, wherein the monomers are selected from the group of C₂ to C₁₆ olefins and mixtures thereof.

23. (Amended) The method according to [any of the preceding claims]claim 1, wherein the monomer is selected from the group of ethylene, propylene, 1-butene, 4-methyl-1-pentene, 1-hexene, dienes, and cyclic olefins, and mixtures thereof.

24. (Amended) The method according to [any of the preceding claims]claim 1, wherein the polymer that is continuously withdrawn is either directly or indirectly fed into another gas phase reactor.

25. (Amended) The method according to [any of claims 14 to 24]claim 14, wherein the collecting vessel is connected to a gas separator, said polymer powder being pneumatically conducted from the collecting vessel to the gas separator.